

Turbulence models in *Code_Saturne*

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Boussinesq approximation

The turbulence viscosity approximation introduced by Boussinesq in 1877 states that the deviatoric Reynolds stress is proportional to the mean rate of strain, that is:

$$-\rho \langle u'_i u'_j \rangle + \frac{2}{3} \rho k \delta_{ij} = \rho \nu_t \left(\frac{\partial \langle U_i \rangle}{\partial x_j} + \frac{\partial \langle U_j \rangle}{\partial x_i} \right) \quad (1)$$

- Widely used, only need to find an expression for a scalar ν_t .
- Isotropic formulation, assumes homogeneity.
- Solid boundaries introduce anisotropy!

Zero and one equation models

- Determine ν_t by prescribing a length scale l (Prandtl, 1925)

$$\nu_t = l^2 \left| \frac{du}{dy} \right| \quad (2)$$

l related to the flow thickness δ , round jet $l/\delta \approx 0.075$, plane jet $l/\delta \approx 0.09$ wall flows $l = \kappa y$

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- Calculate a transport equation for ν_t . The Spalart-Allmaras model uses a transport equation for the viscosity including eight closure coefficients and three damping functions.

Two-equation models

- Calculate the length scale as a ratio of two variables, usually the turbulent kinetic energy (k) and the dissipation (ε) or the rate of dissipation (ω). Solve transport equations for them.

$$k = \frac{1}{2} \langle u'_i u'_i \rangle \quad \varepsilon_{ij} = -2\nu \left\langle \frac{\partial u'_i}{\partial x_k} \frac{\partial u'_j}{\partial x_k} \right\rangle \quad \omega \sim \frac{\varepsilon}{k} \quad (4)$$

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- These are considered complete models, no need to to have prior knowledge of the flow.
- Transport equations are NOT exact, always there is the need to model another term therefore approximations still needed.

k equation

The equation for the turbulent kinetic energy can be derived from the Navier-Stokes equations by multiplying the fluctuating momentum equation by u'_j .

$$\frac{\partial k}{\partial t} + \langle U_j \rangle \frac{\partial k}{\partial x_j} = P_k - \varepsilon + \frac{\partial}{\partial x_j} \left[\left(\nu + \frac{\nu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] \quad (5)$$

with

$$P_{ij} = -\langle u'_i u'_k \rangle \frac{\partial \langle U_j \rangle}{\partial x_k} - \langle u'_j u'_k \rangle \frac{\partial \langle U_i \rangle}{\partial x_k} \quad \text{modelled as} \quad P_k = 2\nu_t S_{ij} S_{ij} \quad (6)$$

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$$\frac{\partial \epsilon}{\partial t} + \langle U_j \rangle \frac{\partial \epsilon}{\partial x_j} = C_{\epsilon 1} \frac{P_k \epsilon}{k} - C_{\epsilon 2} \frac{\epsilon^2}{k} + \frac{\partial}{\partial x_j} \left[\left(\nu + \frac{\nu_t}{\sigma_\epsilon} \right) \frac{\partial \epsilon}{\partial x_j} \right] \quad (7)$$

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- Turbulent viscosity $\nu_t = C_\mu k^2 / \varepsilon$
- Constants calibrated to match SOME experiments (decaying turbulence, free shear flows ...)

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- $k - \omega$ Similar to $k - \varepsilon$ but can be integrated all the way down to the wall (although erroneous profiles for turbulent variables). Easy to converge but free-stream dependent.

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- SST (Shear Stress Transport): Combines $k - \varepsilon$ and $k - \omega$ via empirical functions based on the distance to the wall.
- Spallart-Allmaras: Solves a transport equation for ν_t . Very empirical, tuned for aerodynamic applications.

Keyword in *Code_Saturne*: **iturb**

- **10**: Mixing length.
User needs to prescribe the reference length of the problem.
- **20**: $k - \varepsilon$ (Jones and Launder, 1972).
- **21**: $k - \varepsilon$ with linear production (Guimet and Laurence, 2002).
Production ($P_k = 2\nu_t S_{ij} S_{ij}$) is limited to a linear dependency on S_{ij} . Important in impingement regions.
- **60**: Shear Stress transport, SST (Menter 1994).
Mixes $k - \omega$ near the wall and $k - \varepsilon$ far away. Also has a limiter on the turbulent viscosity.

... In *Code_Saturne*

- **ideuch**: Type of wall function used for the wall boundary conditions (if k is available, u_k can be calculated).
- **igrake**: Whether gravity should be taken into account in the production term.
- **ikecou**: Coupling of the source terms of $k - \varepsilon$.
- **iclkep**: Clipping of negative values.
- **relaxv**: Relaxation factors for each variable.

Reynolds Stress equation

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- From the Navier-Stokes equation:

$$\frac{\partial \langle u'_i u'_j \rangle}{\partial t} + \langle U_k \rangle \frac{\partial \langle u'_i u'_j \rangle}{\partial x_k} = D_{ij}^\nu + D_{ij}^T + \phi_{ij} + P_{ij} + \epsilon_{ij} \quad (8)$$

$$D_{ij}^\nu = \nu \frac{\partial^2 \langle u'_i u'_j \rangle}{\partial x_k \partial x_k} \mathbf{P}_{ij} = -\langle u'_i u'_k \rangle \frac{\partial \langle U_j \rangle}{\partial x_k} - \langle u'_j u'_k \rangle \frac{\partial \langle U_i \rangle}{\partial x_k} \quad (9)$$

$$D_{ij}^T = -\frac{\partial}{\partial x_k} \left(\langle u'_i u'_j u'_k \rangle + \left\langle \frac{p'}{\rho} u'_j \right\rangle \delta_{ik} + \left\langle \frac{p'}{\rho} u'_i \right\rangle \delta_{jk} \right) \quad (10)$$

$$\phi_{ij} = -\frac{1}{\rho} \left\langle p' \frac{\partial u'_i}{\partial x_j} \right\rangle - \frac{1}{\rho} \left\langle p' \frac{\partial u'_j}{\partial x_i} \right\rangle \quad \epsilon_{ij} = -2\nu \left\langle \frac{\partial u'_i}{\partial x_k} \frac{\partial u'_j}{\partial x_k} \right\rangle \quad (11)$$

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$$\phi_{ij} = -c_2 \left(P_{ij} - \frac{2}{3} P_k \delta_{ij} \right) - c_1 \frac{\varepsilon}{k} \left(\langle u'_i u'_j \rangle - \frac{2}{3} k \delta_{ij} \right) \quad (12)$$

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- More complex models (SSG, quadratic, cubic ...etc)
- Not treated the viscous sublayer yet!!

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- **30**: Launder, Reece and Rodi, LLR (Launder et. al, 1975)
Diffusion term modelled by GGDH.
- **31**: Speziale, Sarkar and Gatski, SSG (Speziale et. al, 1991)
Diffusion term modelled by SGDH.

Near wall modelling

Why modelling the near-wall region?

- In the near-wall region, viscosity and non-homogeneities are dominant.

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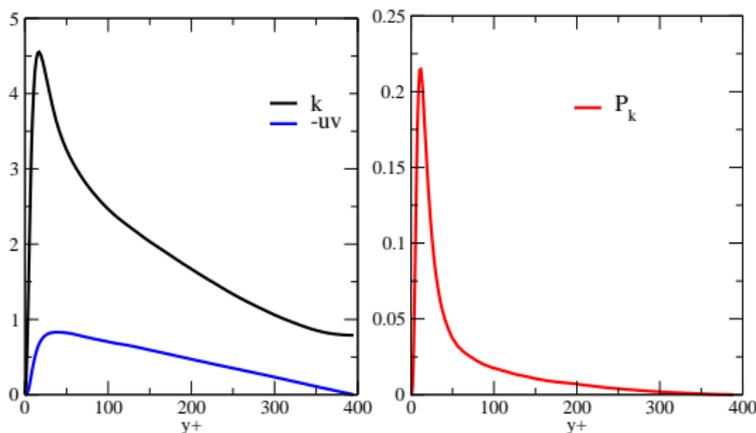
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- The wall normal fluctuations are reduced therefore reducing mixing.

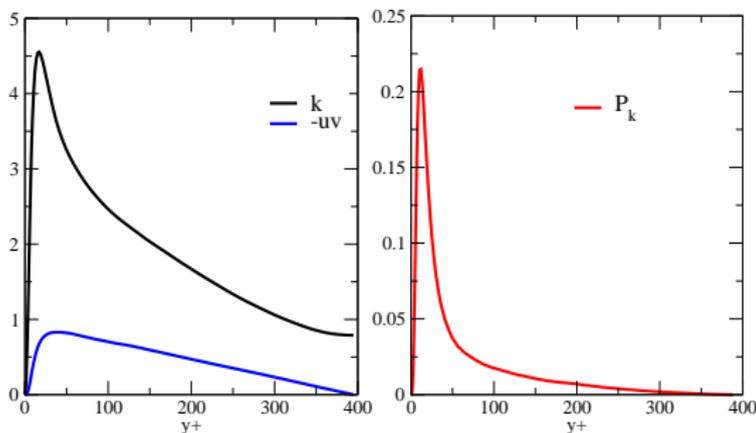
The wall effects

- No-slip: The boundary condition on the mean velocities creates large gradients where the turbulent production originates.



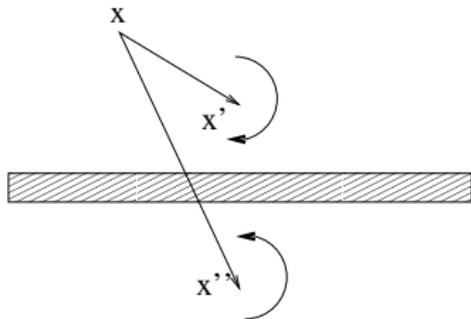
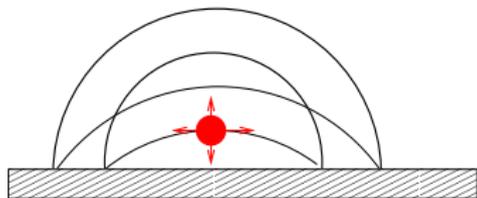
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- Low Reynolds number effects: Interaction between energetic and dissipative scales.



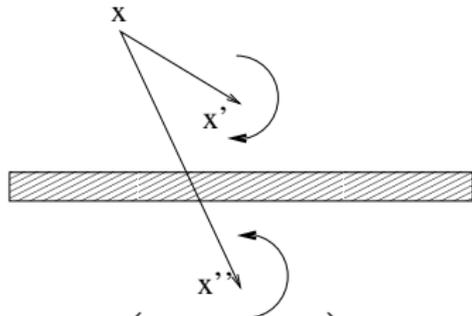
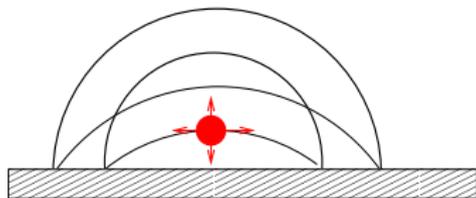
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- Wall echo: Image term in Green's function at the other side of the wall produces an increase in the pressure.

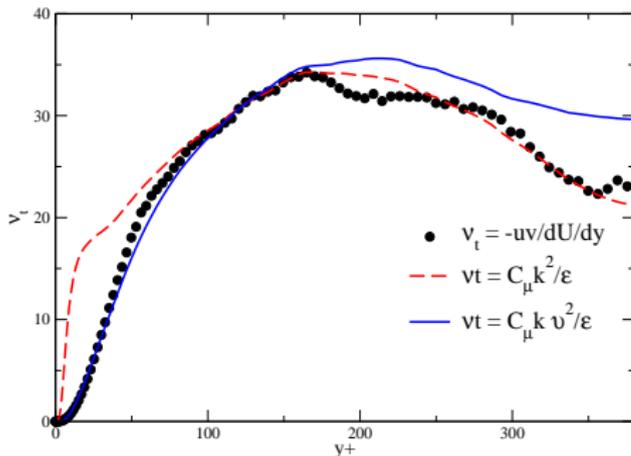


$$p^i(\mathbf{x}, t) = -\frac{1}{4\pi} \int_{-\infty}^{\infty} \int_0^{\infty} \int_{-\infty}^{\infty} S(\mathbf{x}', t) \left(\frac{1}{|\mathbf{r}'|} + \frac{1}{|\mathbf{r}''|} \right) d\mathbf{x}'$$

The $\overline{v^2} - f$ model

In order to simplify the RSM, the elliptic relaxation is introduced to the eddy viscosity approximation (Durbin, 1995).

- Use of correct velocity scale near the wall, $\nu_t = C_\mu \overline{v^2} T$



The $\overline{v^2} - f$ model

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- Reproduces the correct behaviour of the turbulent viscosity near the wall

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- Stiffness of the boundary condition makes it necessary to solve $\overline{v^2} - f$ coupled.

Keyword in *Code_Saturne*: **iturb=50**.

Instead of solving $\overline{v^2}$, a transport equation is solved for the ratio $\varphi = \overline{v^2}/k$ (Laurence et al., 2004):

$$\frac{D(\overline{v^2}/k)}{Dt} = f - \frac{(\overline{v^2}/k)}{k} \mathcal{P} + \frac{\partial}{\partial x_k} \left[\left(\nu + \frac{\nu_t}{\sigma_{(\overline{v^2}/k)}} \right) \frac{\partial(\overline{v^2}/k)}{\partial x_k} \right] + X$$

Where X is the "cross diffusion" term from the transformation:

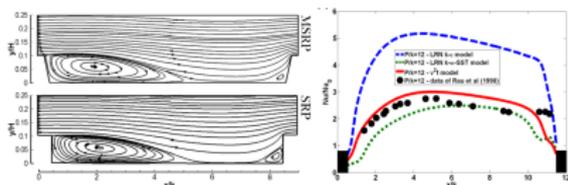
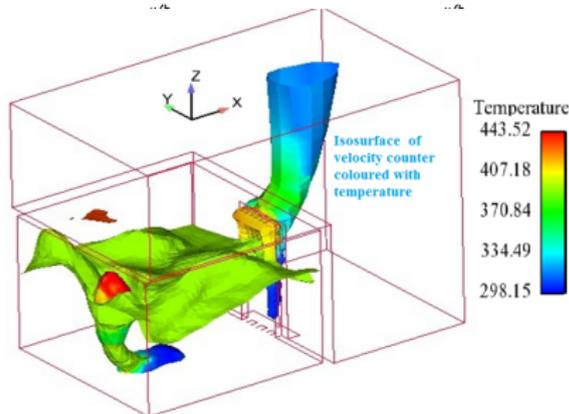
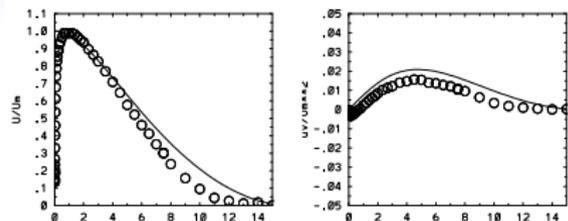
$$X = \frac{2}{k} \left(\nu + \frac{\nu_t}{\sigma_{(\overline{v^2}/k)}} \right) \frac{\partial(\overline{v^2}/k)}{\partial x_k} \frac{\partial k}{\partial x_k}$$

Which one to choose?

... It depends on the case.

EVMs

- Fast and robust.
- Can be used with wall functions to save CPU.
- Simple and easy to understand.
- Basic assumptions.
- Do not take into account anisotropy.
- limitations in flows with impingement, rotation, curvature, separation ...

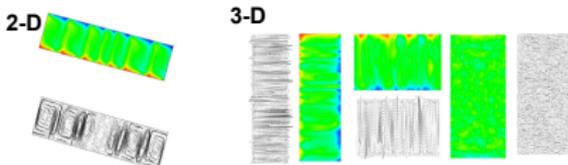
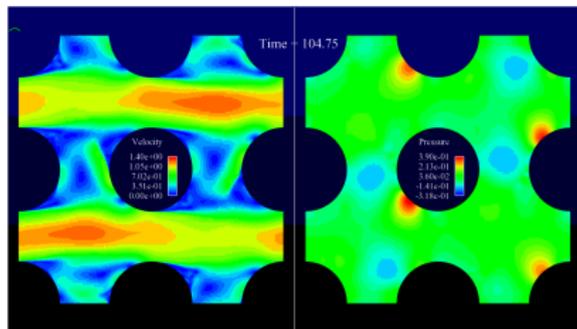
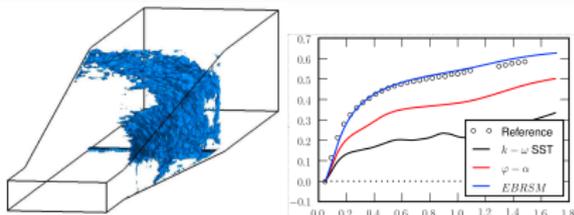


Which one to choose?

... and on the CPU available.

SMCs

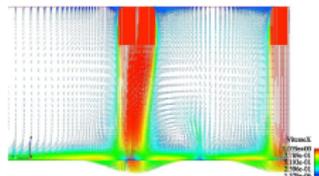
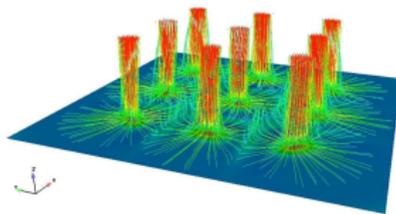
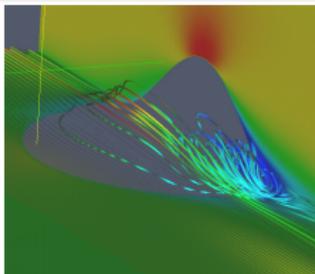
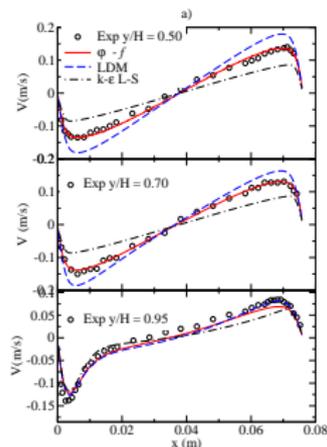
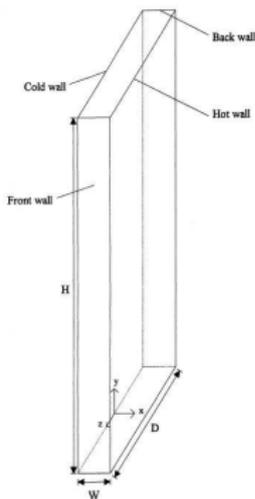
- More physics involved.
- Full anisotropic model.
- Exact production term.
- Better for 3D and unsteady flows.
- More equations
($u, v, w, p, \overline{u_i u_j}, \varepsilon$)
- More CPU.
- Can have convergence difficulties.



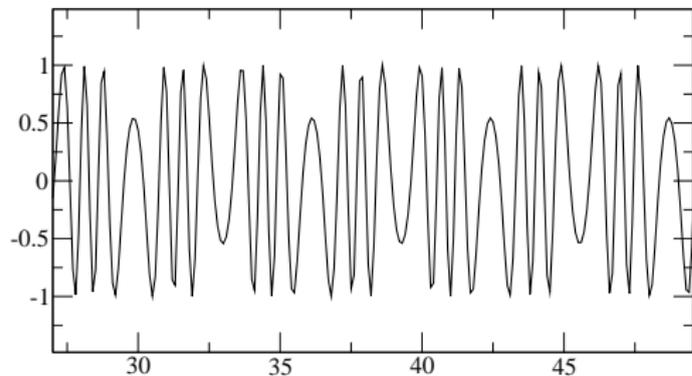
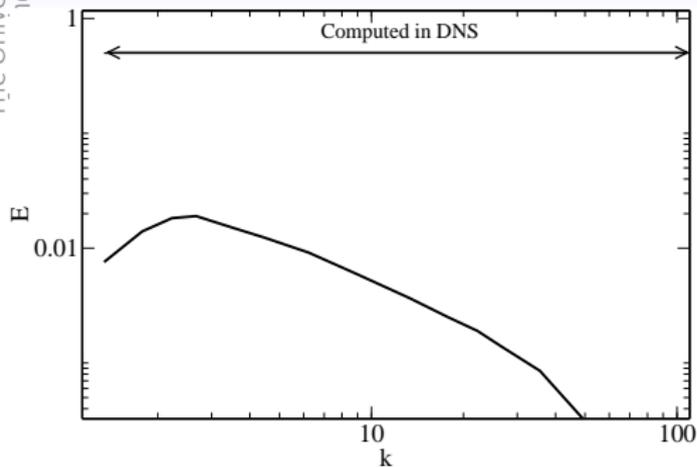
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Low-Re models

- Near wall region is important.
- Where friction coefficient or heat transfer are not in the log-law.
- Separated flows.
- Wall induced anisotropy.



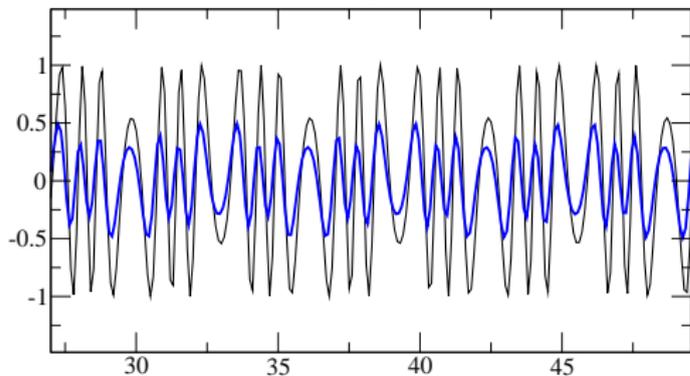
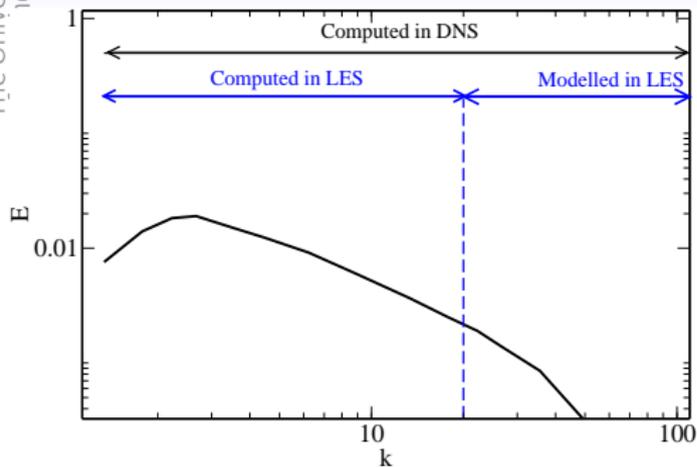
Large Eddy Simulation



Turbulent flows simulations

- Take the instantaneous signal and filter it.

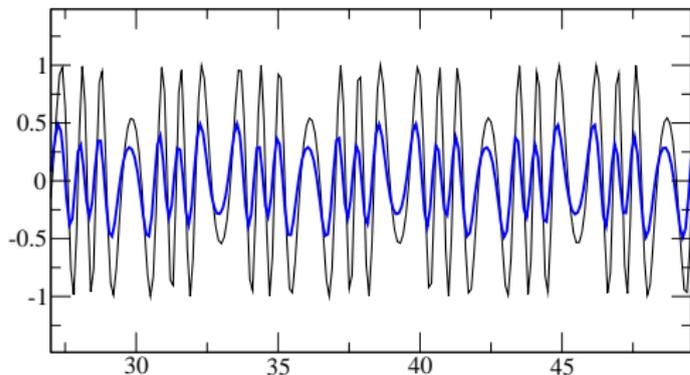
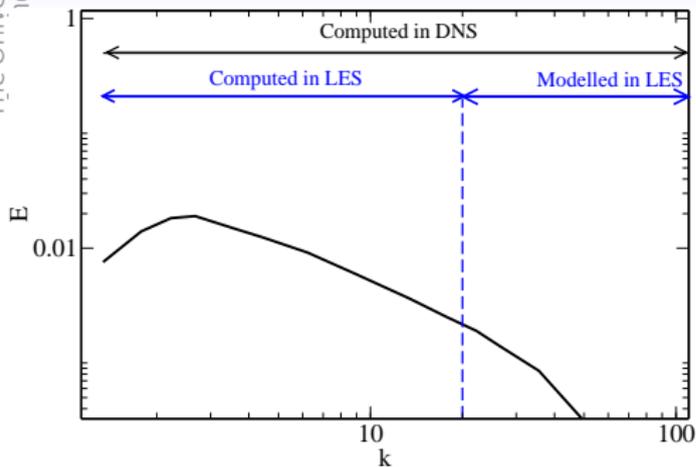
Large Eddy Simulation



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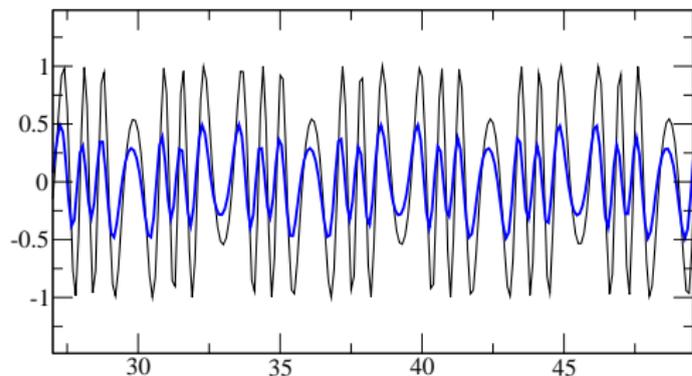
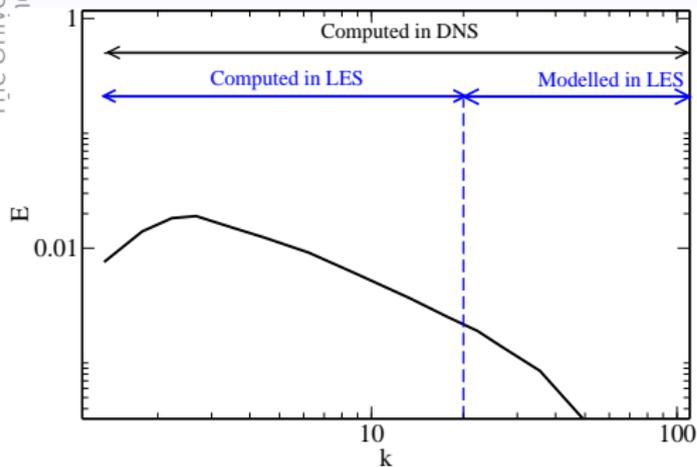
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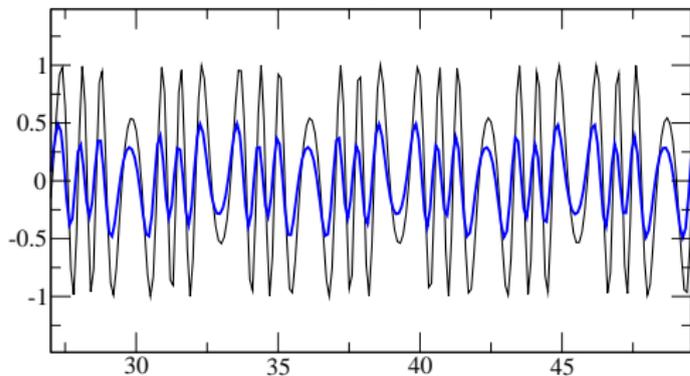
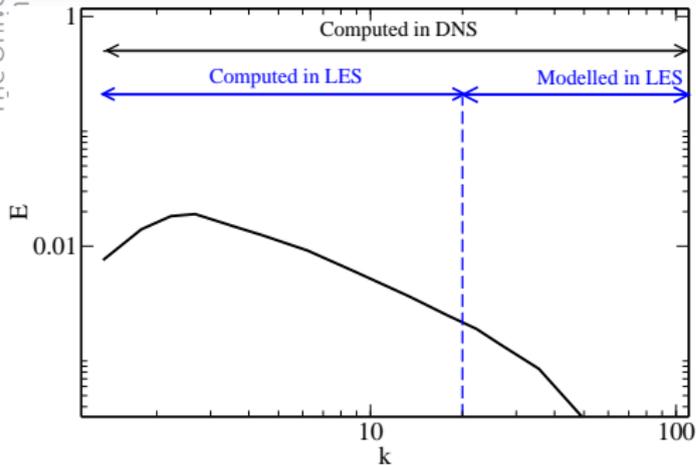
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- But they tend to be more homogeneous and easier to model.

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- Requires very fine meshes near the solid boundaries.
- To get mean values, simulation needs to run long enough.

By filtering the Navier-Stokes equations and unknown term arises:

$$\tau_{ij}^R = \overline{U_i U_j} - \overline{U_i} \overline{U_j} \quad (13)$$

- Assume all scales inside the filter width (Δ) are homogeneous.
- Homogeneous scales are easier to model.
- In practice, $\Delta = 2Vol^{1/3}$.
- Which means that to treat in-homogeneous regions Δ needs to be reduced.
- Smaller $\Delta \rightarrow$ smaller cells \rightarrow higher number of cells needed.
- Classical example: Wall bounded flows.

The Smagorinsky (1964) model

Introduce a turbulent viscosity so that:

$$\tau_{ij} - \frac{2}{3}\tau_{kk}\delta_{ij} = 2\nu_t S_{ij} \quad (14)$$

with

$$\nu_t = (C_s \Delta)^2 \sqrt{2S_{ij}S_{ij}} \quad \text{with} \quad S_{ij} = \frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) \quad (15)$$

Here C_s is a “constant”. Theoretical value $C_s \approx 0.17$ but in reality it is adapted to the flow (e.g. Wall bounded flows use $C_s \approx 0.065$).

- ν_t doesn't vanish in laminar sublayer or transitional flows (and it should!).
- Van Driest damping is used in wall bounded flows
 $f_\mu = 1 - \exp(-y^+/A^+)$

Dynamic Smagorinsky (Germano, 1991)

Since the C_s is not constant, try to compute it dynamically for each flow.

- Use a second test filter and apply it to the filtered velocity field $U = \widetilde{\widetilde{U}} + (\overline{U} - \widetilde{\widetilde{U}}) - u'$
- Then compute from the velocity field: $\mathcal{L}_{ij} = \widetilde{\widetilde{U_i U_j}} - \widetilde{\widetilde{U_i}} \widetilde{\widetilde{U_j}}$
- Compute $M_{ij} \equiv 2\overline{\Delta}^2 \widetilde{\widetilde{S S_{ij}}} - 2\widetilde{\widetilde{\Delta}}^2 \widetilde{\widetilde{S}} \widetilde{\widetilde{S_{ij}}}$
- The mean-square error is minimised (Lilly 1992) by specifying:
 $c_s = M_{ij} L_{ij} / M_{kl} M_{kl}$

WALE model (Nicoud & Ducros, 1999)

Wall Adapting Local Eddy viscosity.

- Need to correct the near wall behaviour of the SGS models.
- Usually done by Van Driest damping but this requires y and u_τ
- Find a way to mimic the asymptotic behaviour:

$$\nu_t = (C_s \Delta)^2 \frac{(S_{ij}^d S_{ij}^d)^{2/3}}{(S_{ij} S_{ij})^{5/2} + (S_{ij}^d S_{ij}^d)^{5/4}} \quad (16)$$

with $S_{ij}^d = S_{ik} S_{kj} + \Omega_{ik} \Omega_{kj} - \frac{1}{3} (S_{mn} S_{mn} - \Omega_{mn} \Omega_{mn}) \delta_{ij}$

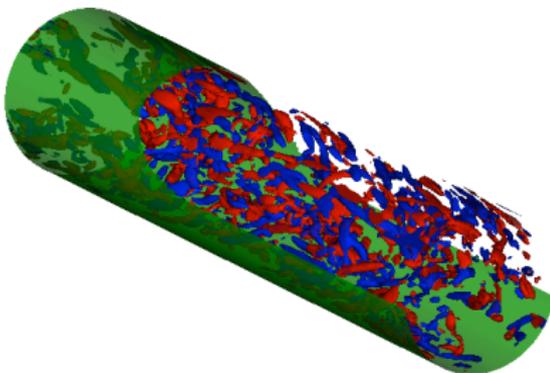
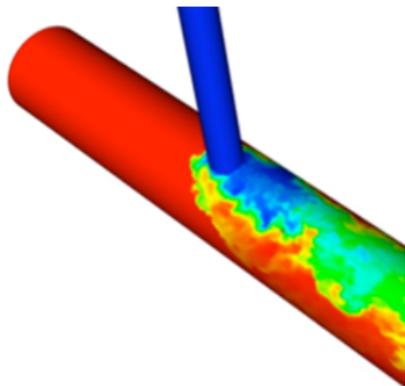
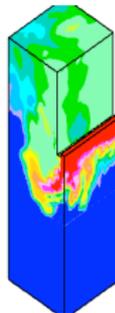
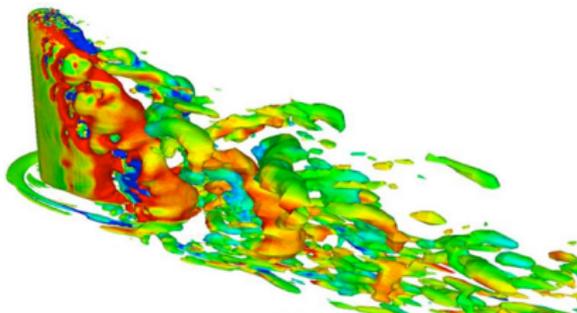
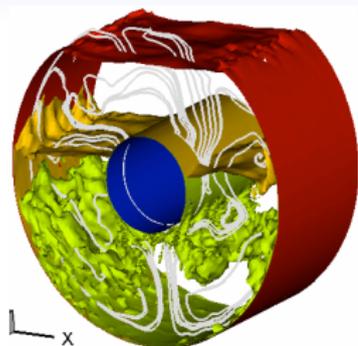
Keyword in *Code_Saturne*: **iturb**.

- **40**: Smagorinsky. Thoroughly tested but C_s case dependant.
- **41**: Dynamic. Useful when laminar regions are present (walls, transition, natural convection). Requires finer meshes (two filters). Negative ν_t might appear.
- **42**: WALE. No need for wall damping. Correct asymptotic behaviour. Not very popular.

When using LES ...

- Well resolved LES results often better than RANS but coarse LES worst than coarse RANS.
- Numerical issues are very important. Second order in time and space required.
- Need to extract statistical values to have any meaning.
- Meshing is very important. Need to know the scales in the flow so a precursor RANS simulation is very helpful.
- Cell distortion, high aspect ratio and excessive growth should be avoided.

LES examples



Pictures from: Y.Addad, S. Benhamadouche and I. Afgan

Hybrid methods

When flow is too complex for RANS (EVMs or SMCs) and the mesh requirements for LES are too large ($\Delta y^+ \sim 1$, $\Delta x^+ \sim 50$, $\Delta z^+ \sim 20$).

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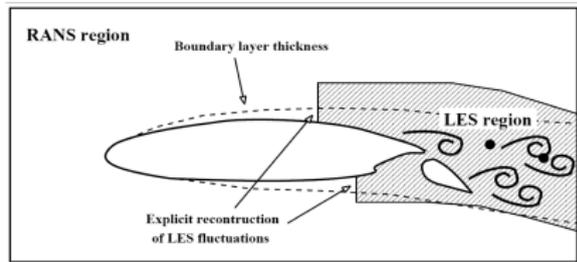
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Interface

Prescribe an interface, one side RANS another LES.

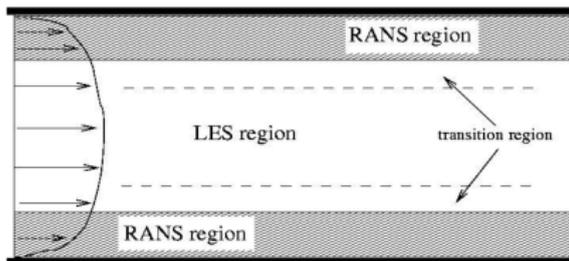
- Needs to add turbulent information when going from RANS to LES.
- Good for streamwise coupling using synthetic turbulence.
- More difficult with wall normal coupling.



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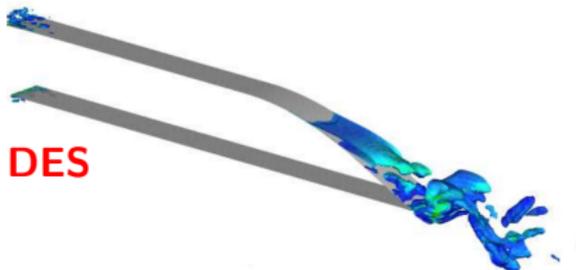
Seamless

Let the model change automatically.

- Needs a parameter to switch from RANS to LES, usually based on the cell size.
- Fluctuations can easily die while in RANS.
- User needs to carefully design the mesh for the appropriate switch to occur.

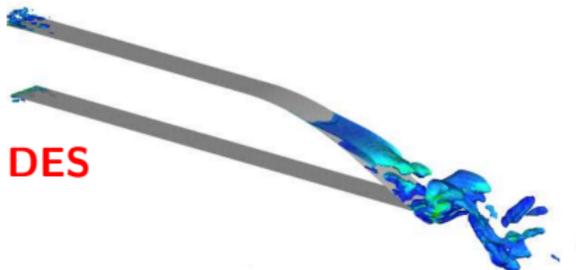
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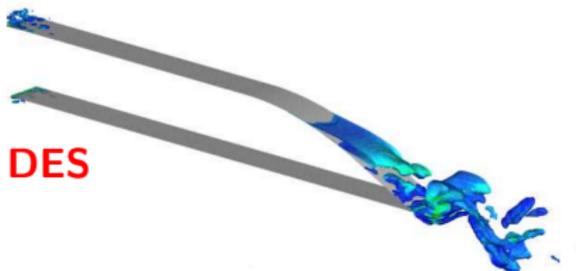
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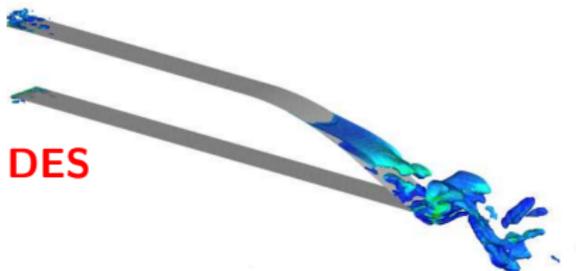
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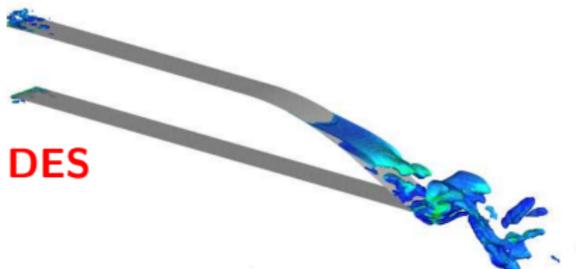
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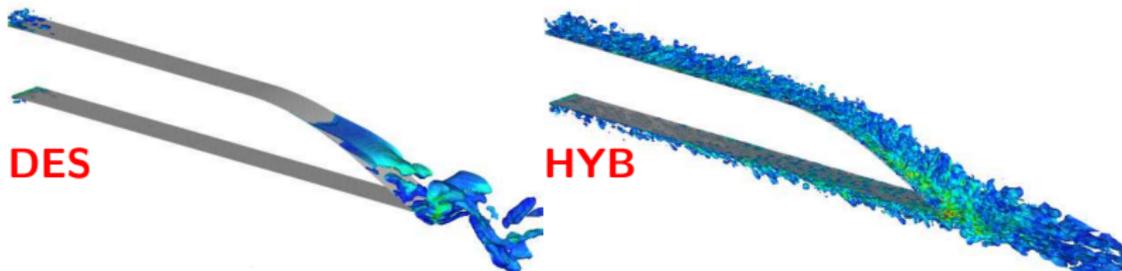
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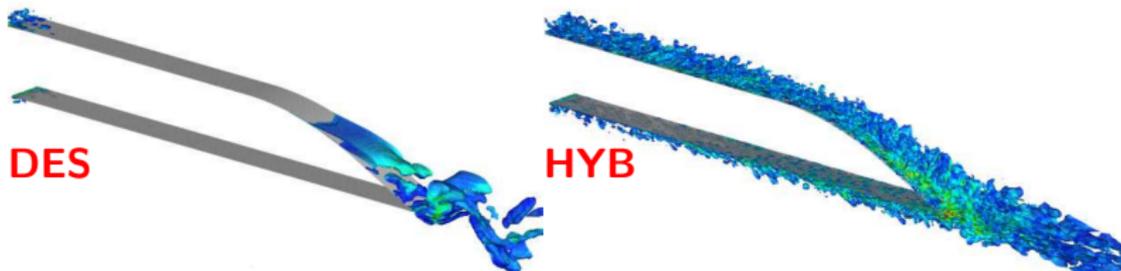
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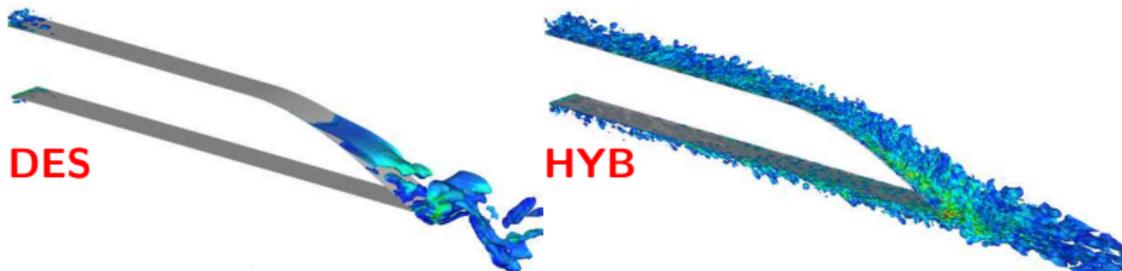
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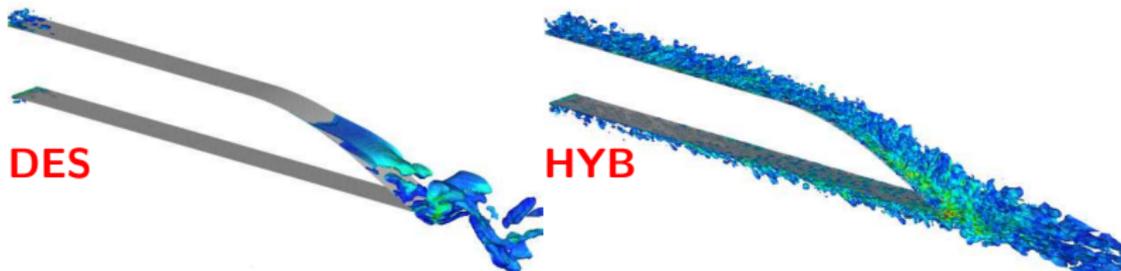
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 - Not as mesh dependent since both models act on the whole domain.

